



Partitioning und Transmutation: Aktueller Stand



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EC-JRC-ITU

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Joint
Research
Centre



transmutation options



- Transmutation of minor actinides (MA) can be achieved by using:
- thermalised neutron facilities (LWRs)
 - fast neutron spectrum facilities,
 - critical reactors or
 - sub-critical accelerator driven systems (ADS)
 - ADS operates in a flexible and safe manner even with a core loading containing a high amount of MA

Comparison of thermal and fast neutron spectrum: ratio of capture σ_c / fission cross sections σ_f

	PWR UOX			FR (EFR)		
Isotope	σ_f	σ_c	$\alpha = \sigma_c / \sigma_f$	σ_f	σ_c	$\alpha = \sigma_c / \sigma_f$
²³⁷ Np	0.52	33	63	0.32	1.7	5.3
²⁴¹ Am	1.1	110	100	0.27	2.0	7.4
²⁴³ Am	0.44	49	111	0.21	1.8	8.6
²⁴² Cm	1.14	4.5	3.9	0.58	1.0	1.7
²⁴³ Cm	88	14	0.16	7.2	1.0	0.14
²⁴⁴ Cm	1.0	16	16	0.42	0.6	1.4
²⁴⁵ Cm	116	17	0.15	5.1	0.9	0.18
⁹⁹ Tc	/	9	/	/	0.5	/



❑ MYRRHA (SCK•CEN, Belgium)

Multi-purpose hYbrid Research Reactor for High-tech Applications

- Started in 1998
- Projected to be in operation by 2028

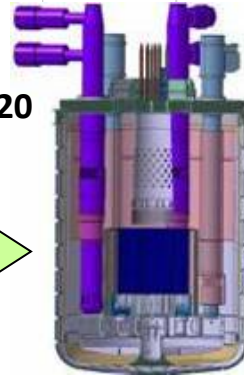
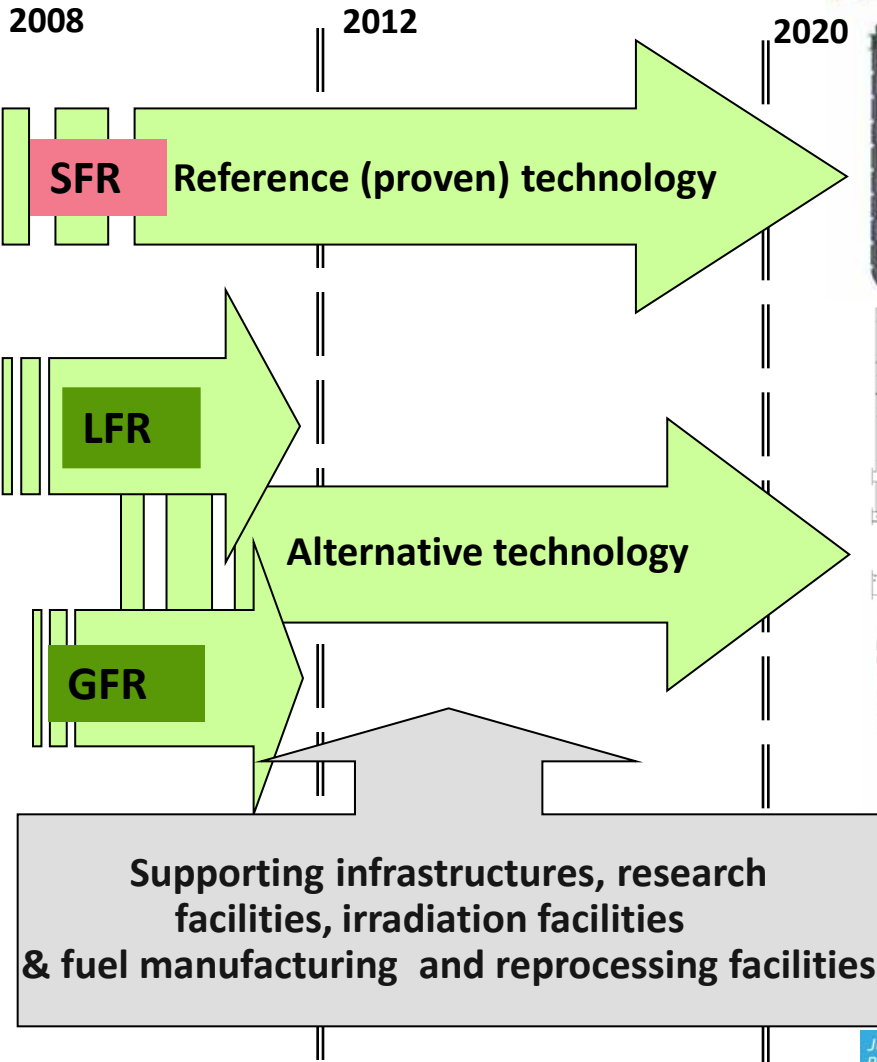
❑ EC 6th Framework programme EUROTRANS

- XT-ADS
- EFIT_Pb
- EFIT_Gas (back up)

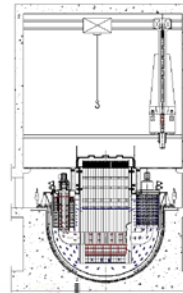


A fast spectrum testing facility in Europe, beyond 2015 complementary to Jules Horowitz Reactor (F).

ESNII strategy



**SFR Prototype
Astrid
250-600 MWe**

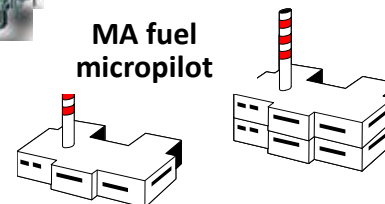


**LFR
demonstrators
MYRRHA
ALFRED**



Allegro GFR Demo

- Test bed of GFR technologies
- Innovative fuel
- MA transmutation
- Coupling to heat applications



**MA fuel
micropilot**

**MOX fuel
fab unit**

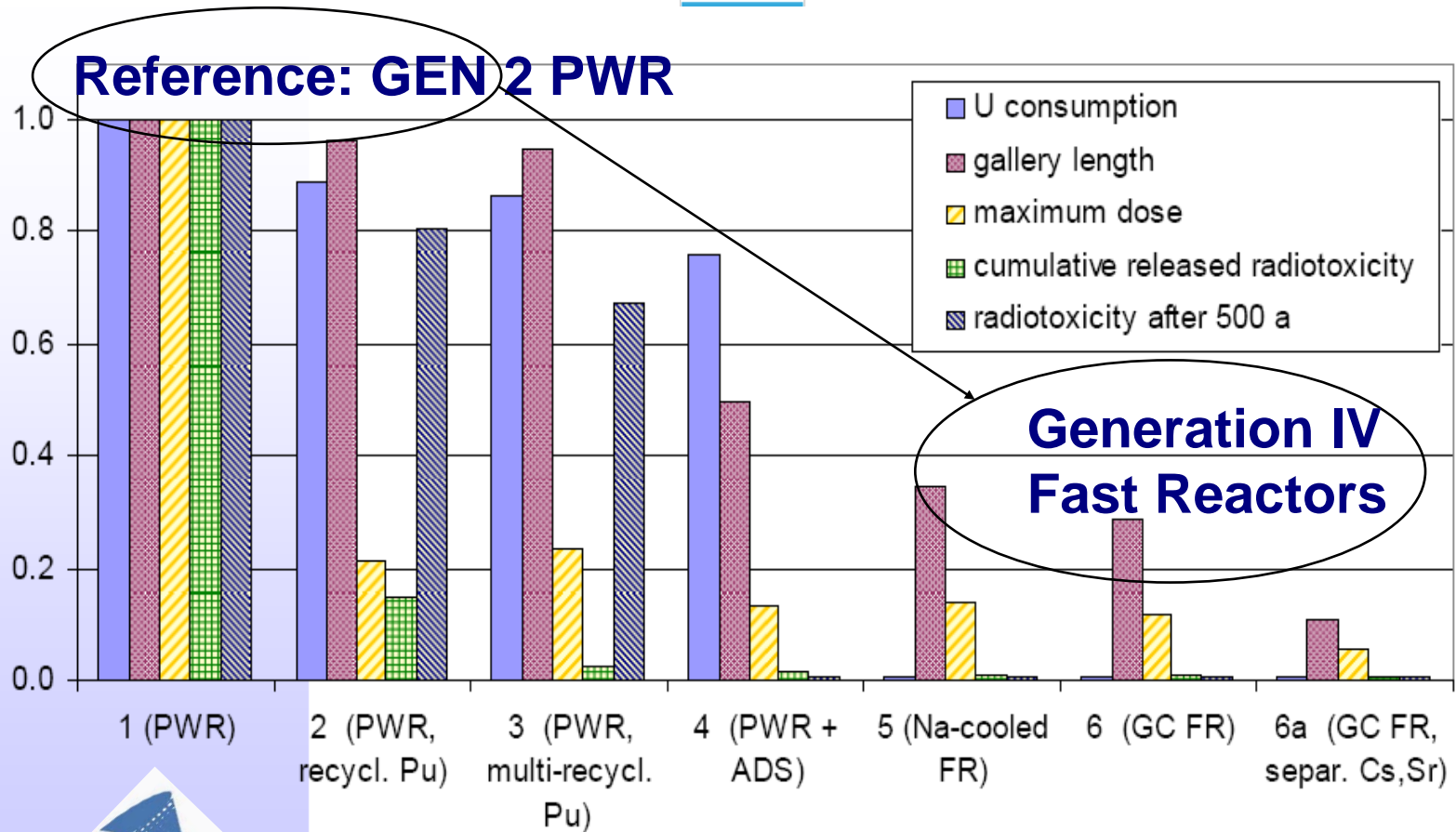
CP ESFR, ESNII +



2040: Target for deployment of Gen-IV Fast Neutron Reactors

or earlier if new energy needs (electric vehicles, process heat applications)

Sustainable fuel cycles vs open LWR cycle



RED-IMPACT main results

Why P&T



- ✓ Improve long-term public safety (reduce radio-toxicity and future doses to man)
- ✓ Repository heat and size (footprint)
- ✓ Reduce the proliferation risk of plutonium in spent fuel
- ✓ Responsibility for own waste production
- ✓ Responsibility towards future generations
- ✓ Full actinide recycling means remote operation (additional risk for operators)

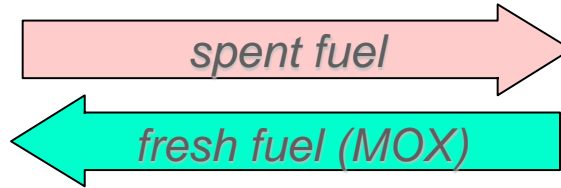
Advanced nuclear fuel cycle double strata concept



commercial reactor
EPR, Olkiluoto, Finland

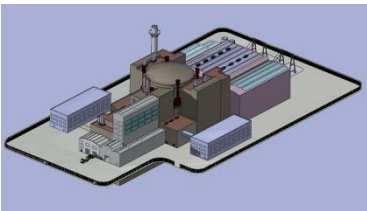


reprocessing plant
La Hague, France



PUREX & advanced aqueous

Integral fast reactor or ADS



ASTRID, France



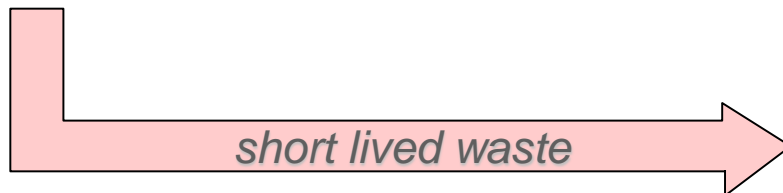
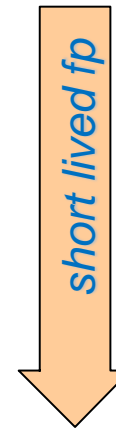
INL, US



MYRRHA, Belgium



multirecycling pyro



waste repository
SFR, Forsmark, Sweden



reasons for selecting pyro-techniques



compact process

Integrated Fast Reactor concept, ANL
lower costs, reduced number of transports

faster recycling

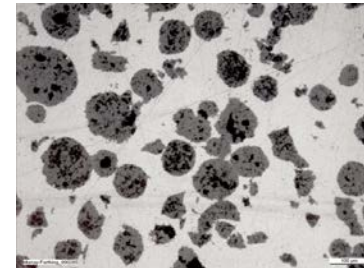
salt more radiation resistant => short fuel
cooling-times

"impure" product fractions

more "proliferation-resistant" process

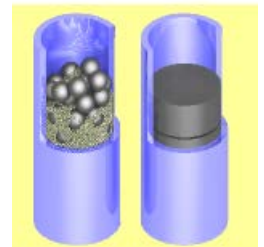
fuel composition

- Metallic fuels, CERMET
- Inert Matrix (MgO , ZrO_2) fuels
- Th - MOX
- Nitrides eventually carbides
- Shpere Pac



$\text{Mo}-(\text{Pu}, \text{Am})\text{O}_2$

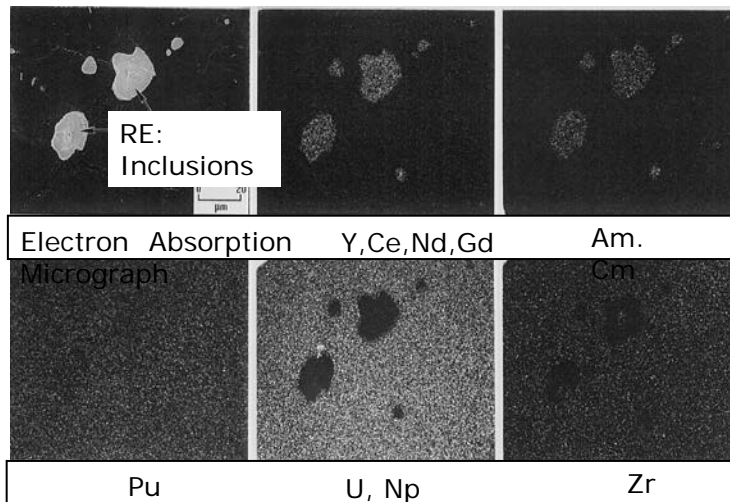
$(\text{U}, \text{Am})\text{O}_2$



reasons for Ln/An separation

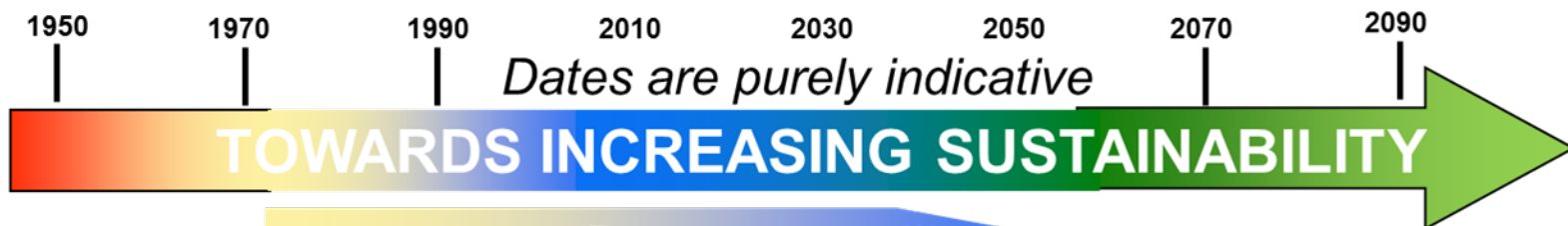


- material burden: in spent LWR fuels, the Ln content is up to 50 times that of Am/Cm
- neutron poisoning: Ln (esp. Sm, Gd, Eu) have very high neutron capture cross sections, e.g. $> 250\,000$ barn for Gd-157
- segregation at fuel fabrication: upon fabrication, Ln tend to form separate phases, which grow under thermal treatment; An concentrate in these phases



electron micrographs of an UPuZrMA5RE5 alloy

⇒ consequence: non-uniform heat distribution in the fuel under irradiation



Gen. II & III ***Pu-monorecycling***

Gen. IV ***Pu-multi-recycling***

Pu-mono-recycling

- PWR reactors
- Pu-recycling in MOX fuel
- from PUREX to COEX™

Pu multi-recycling

- Fast-Reactors (FR)
- Pu multi-recycling
- COEX™ process

Gen. IV ...+ MA recycling

Pu+MA multi-recycling

- Fast Reactors (FR)
- Pu multi-recycling
- MA burning
- MA specific separation processes

Main incentives

- 1st step towards U resource saving
- Efficient waste conditioning

Main incentives

- Major resource saving
- Energetic independence
- Economic stability

Main incentives

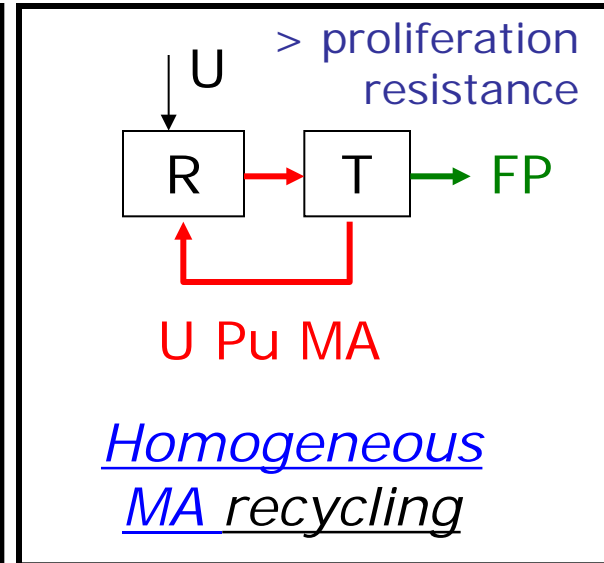
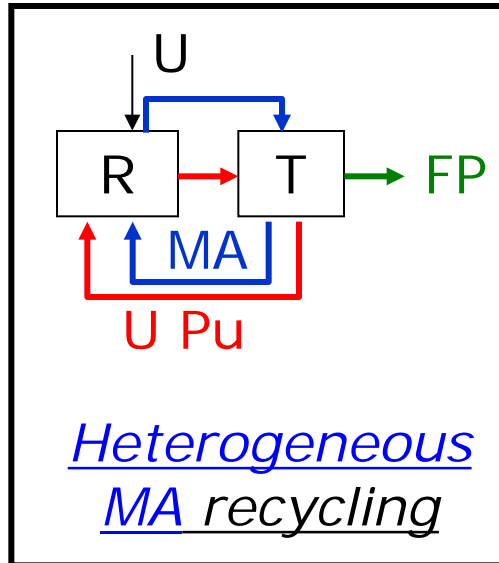
- Decrease of waste burden,
- Optimisation of the disposal
- Public acceptance

Advanced nuclear fuel cycle concepts



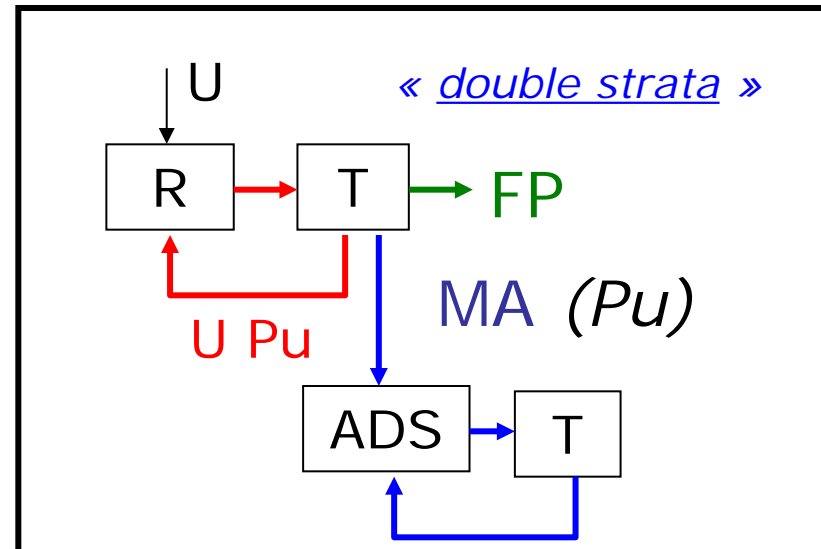
Aqueous reprocessing

- U, Pu, Np recycled PUREX – COEX
- Heterogenous MA by DIAMEX/SANEX
- Homogenous An by GANEX



Aqueous + Pyro reprocessing

- U, Pu recycled by PUREX or COEX
- Heterogenous recycling of MA
- Pyro recycling of targets

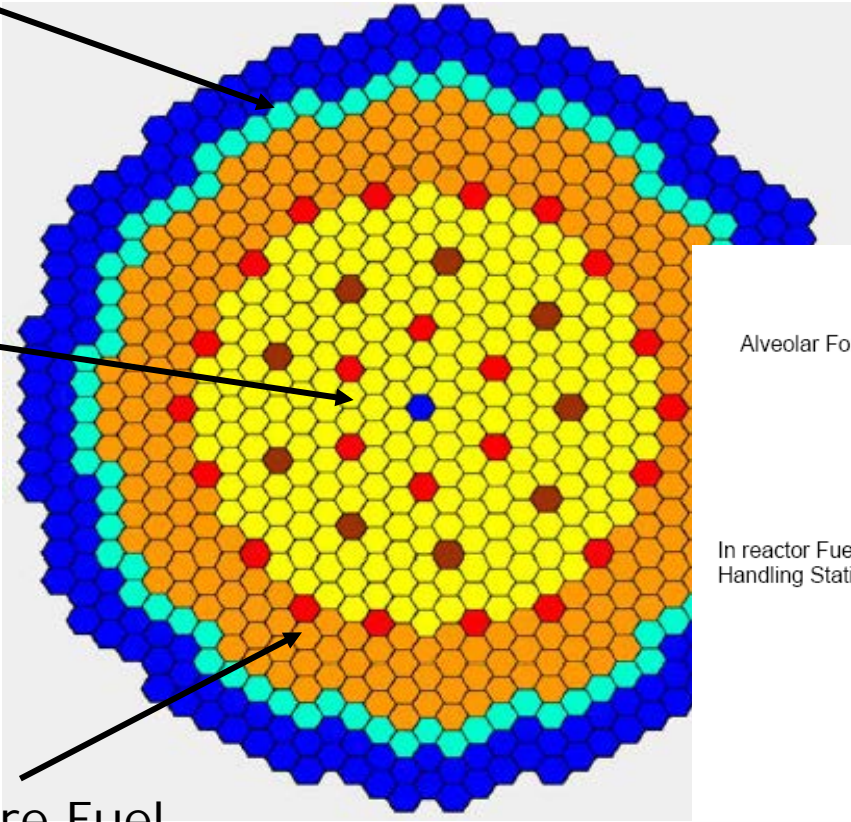


E-SFR concept GIF SFR track

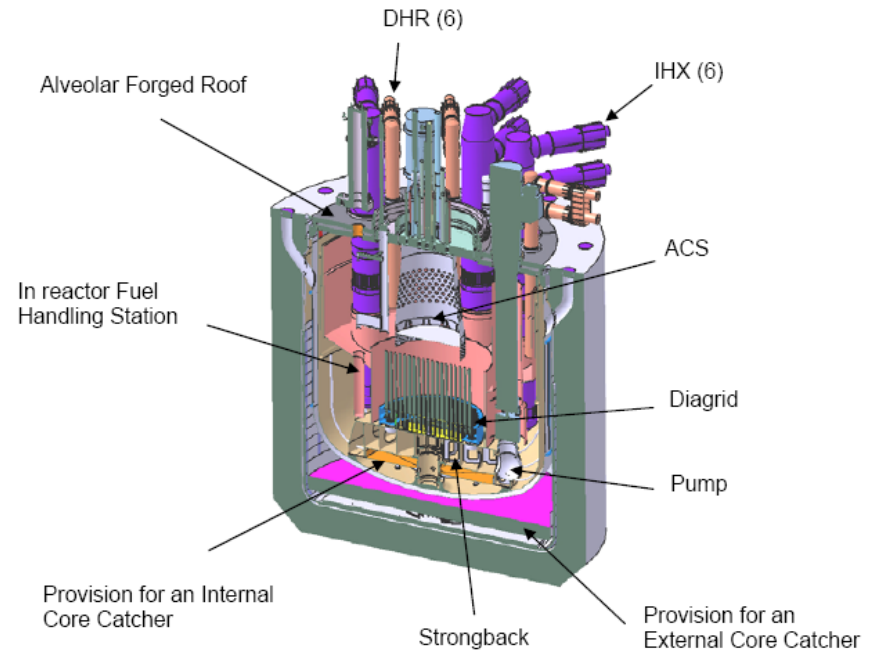
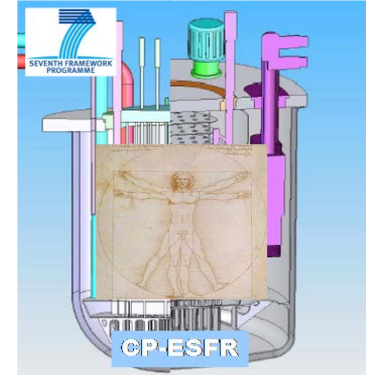


1 Row of
Assemblies
with Minor
Actinides

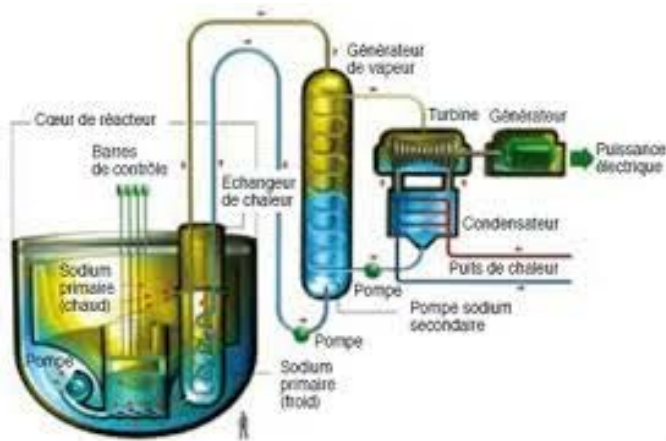
Inner core
Fuel
Assemblies



Outer core Fuel
Assemblies



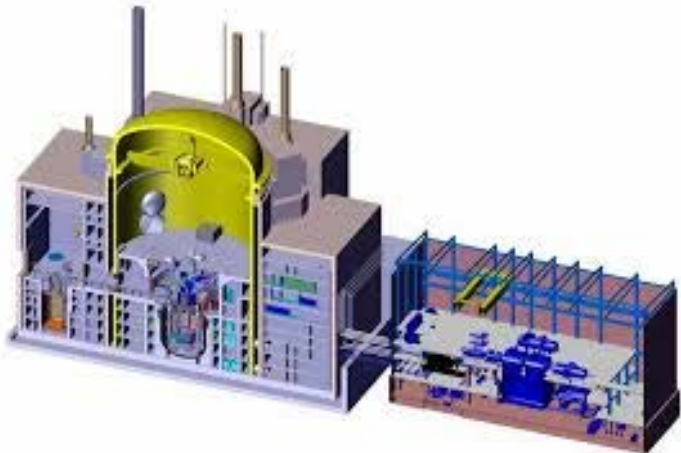
French Astrid project



minor actinide transmutation on an industrial scale:

- Homogeneous concept : 2% of Am in a standard fuel
- Heterogeneous concept : 10% on UO₂ in the radial blanket

Several experimental phases in ASTRID to implement different transmutation scenarios





- 1) Overall P&T efficiency, 99.9%
- 2) Transmutation efficiency, 10% - 20%

→ multi-recycling required

→ Partitioning efficiency > 99.9%

< 0.1% losses

Decontamination factor > 1 000

European partitioning projects



FP3
1990-1994

HLLW partitioning by means of completely incinerable extractants

FP 4
1994-1998

New partitioning techniques for minor actinides, NEWPART



FP5
1998-2002

*Pyrometallurgical reprocessing PYROREP
New Solvent Extraction Processes for
minor actinides, PARTNEW*



FP6
2002-2006

*Partitioning of MA from high active
wastes, EUROPART*



FP7
2007-2013

*Actinide recycling by separation
and Transmutation ACSEPT*



Since 2013

*Safety of ACTinide Separation
proceSSes SACSESS*



TODGA/BTBP experiment



1.5 kg of commercial LWR fuel (60 GWd/tHM)

PUREX process: co-extraction of U, Pu and Np

Denitration and concentration of feed (10x)

- No losses of actinides in precipitate

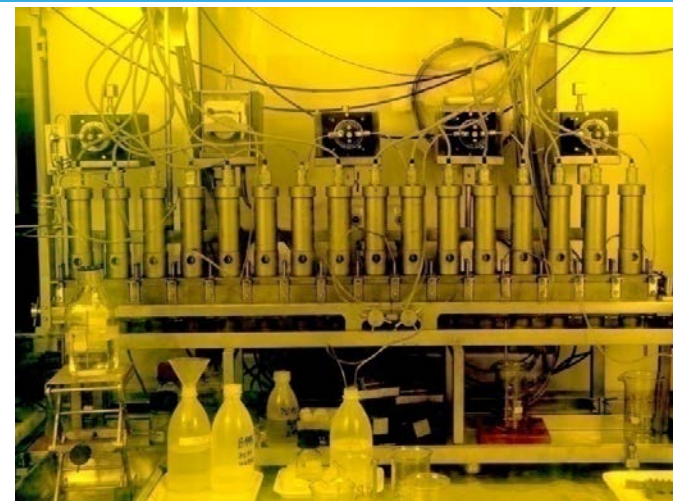
Co-extraction of An and Ln by TODGA/TBP demonstration process from concentrated Purex raffinate

First successful BTBP demonstration process using the genuine TODGA/TBP product as feed

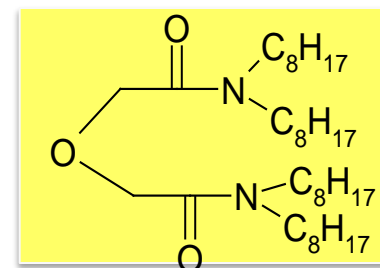
Overall recoveries of all the An ~99.9 %



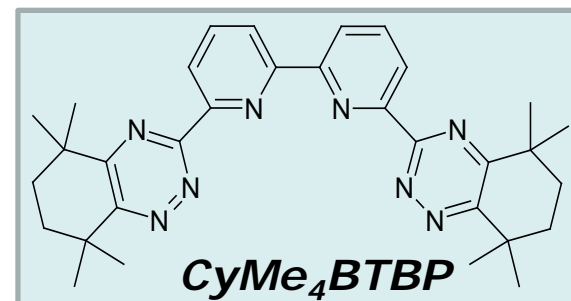
Joint
Research
Centre



**centrifugal contactor
battery**



TODGA



CyMe₄BTBP



SUPERFACT Fuel Cycle Closure



*fuel
characterization*



$(U, Pu, Np, Am)O_2$
 Np : 2-45%, Am : 2-20%



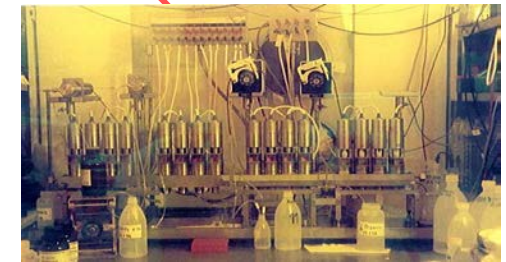
*irradiation (PHENIX)
360 EFPD*



fuel fabrication

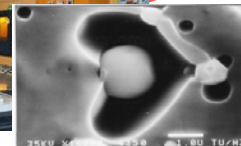
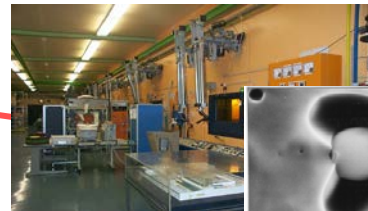


*separated
actinides
(Np , Am , Cm)*



reprocessing

*post irradiation
examination*



*transmutation
rate ~ 30%*



genuine fast reactor fuel



Feed characterisation and adjustment

IC-ICP-MS, TIMS, ICP-MS, titration

Flow-sheet calculations (CEA and NNL)

GANEX 1

Extraction of U leaving
other An in raffinate
Feed ~ 150 – 175 g/L U
2 stage process,
16 stages extraction and
scrubbing
16 stages back
extraction
DEHiBA (monoamide)

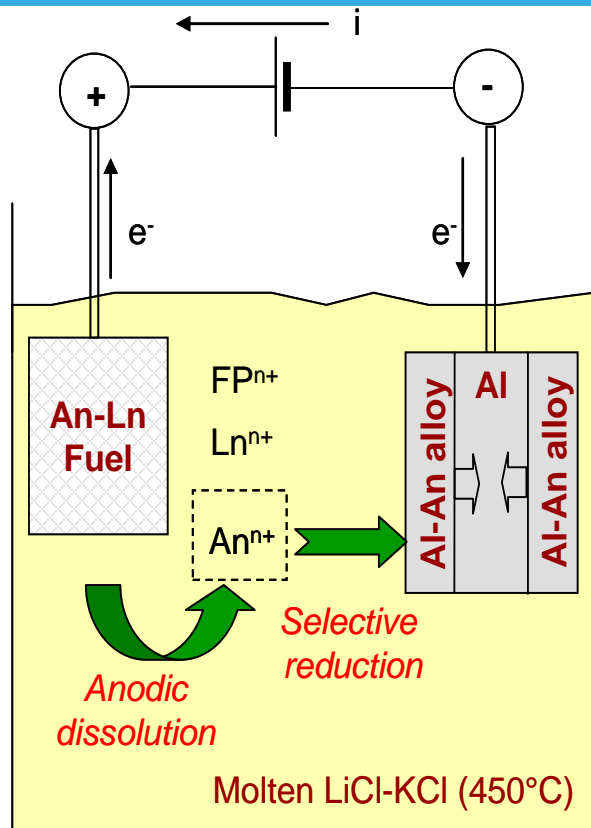
U recovery >99.9%

GANEX 2

Pu, Np and MA extraction
and separation
feed of ~ 15 g/L Pu
2 stage process
16 stages extraction and
scrub
16 stages backextraction
TODGA + DMDOHEMA

grouped TRU recovery
close to 99.9%

Electrorefining on solid aluminium cathode



- **Efficiency**

High efficient grouped separation of all actinides using Al cathode and un-irradiated and irradiated METAPHIX fuel:
 $U_{61}Pu_{22}Zr_{10}Am_2Nd_{3.5}Gd_{0.5}Y_{0.5}Ce_{0.5}$

- **Deposits characterisation**

Solid, compact deposits composed of An-Al alloys (mainly $AnAl_3$, $AnAl_4$)

- **Capacity of Al to take-up An:**

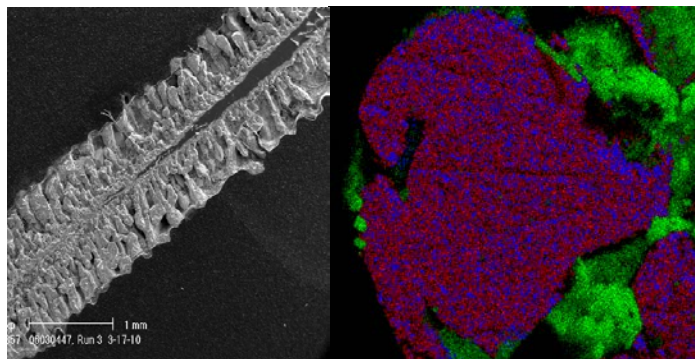
Very high capacity of solid Al demonstrated: More than 2 g of An in 1 g Al

- **Selectivity**

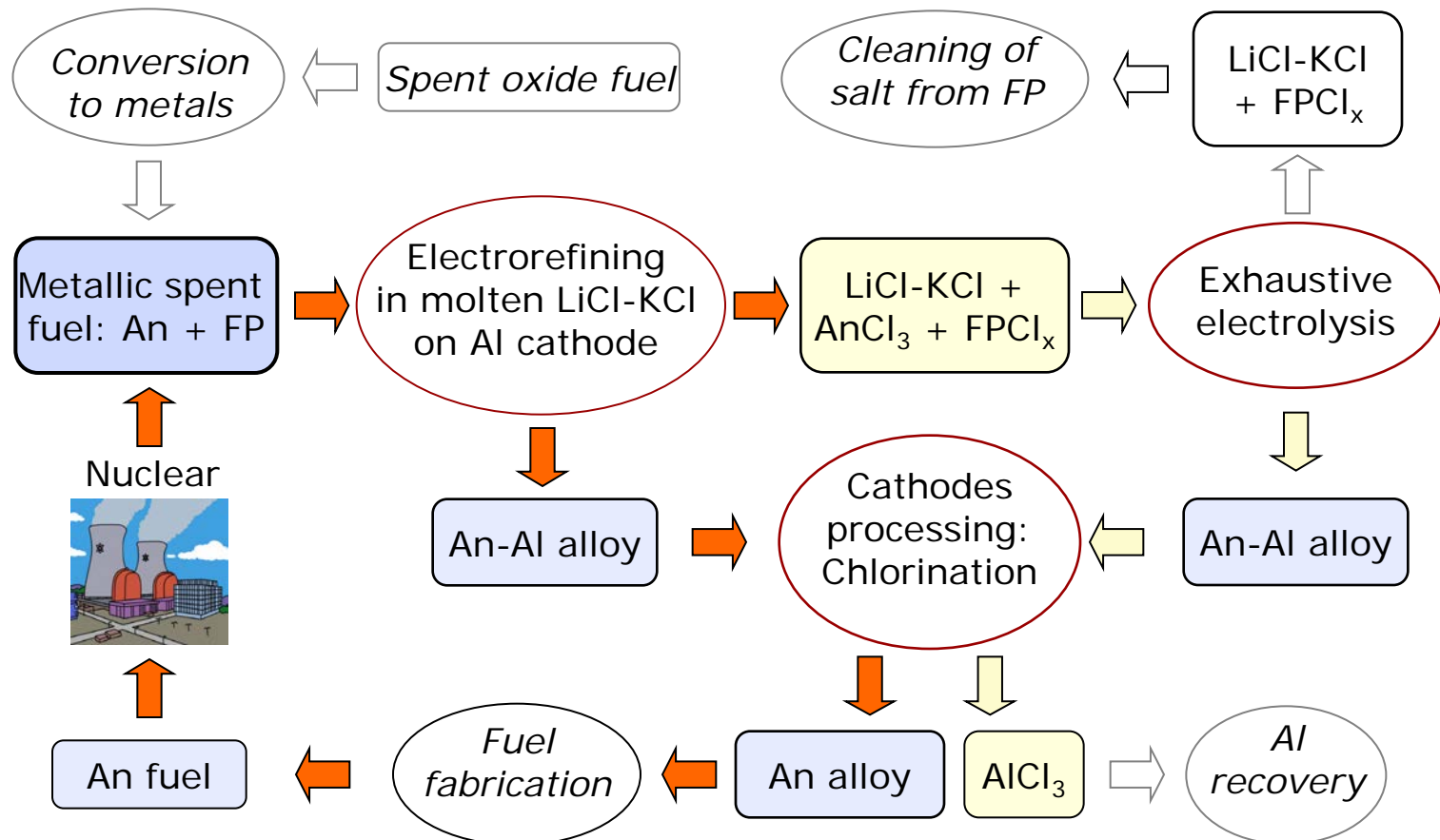
less than 2% lanthanides contained in the actinide deposit

- **Recovery**

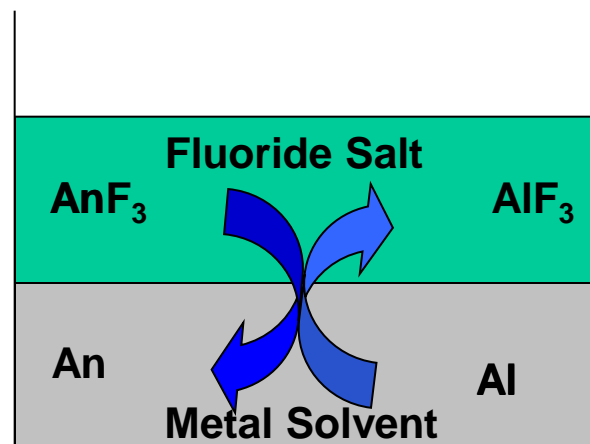
> 99.9% actinide recovery



Pyrochemical Advanced Nuclear Fuel Cycle



CEA liquid metal/molten salt extraction process



Salt before extraction

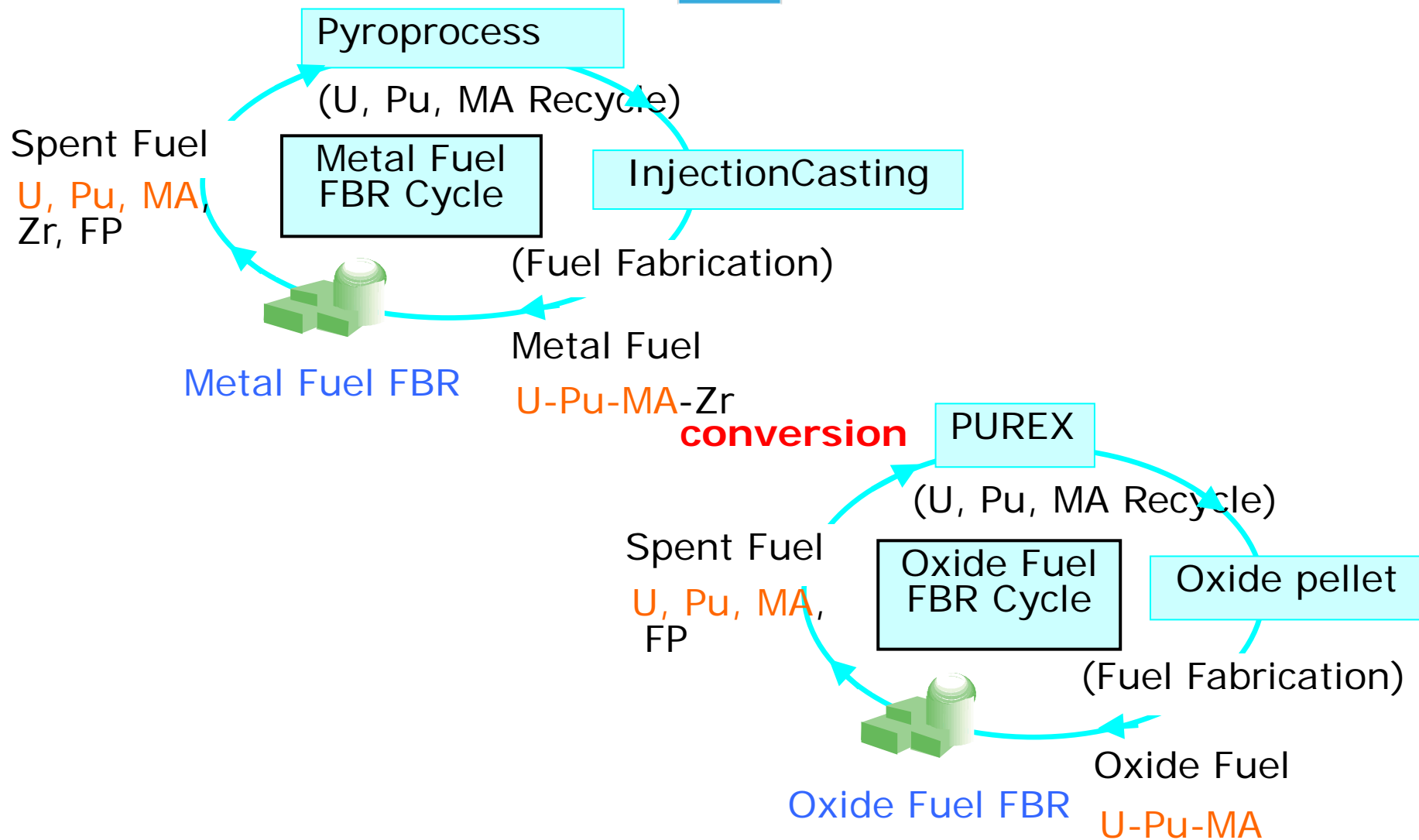


Salt after extraction

Actinide distribution coefficients > 100

An/Ln separation factors > 1000

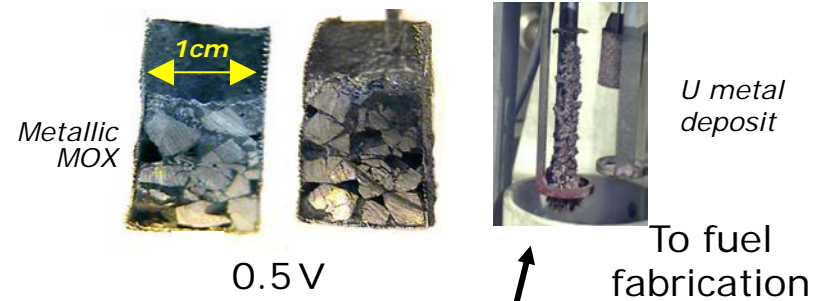
Fuel Conversion



oxide fuel treatment by pyro-process



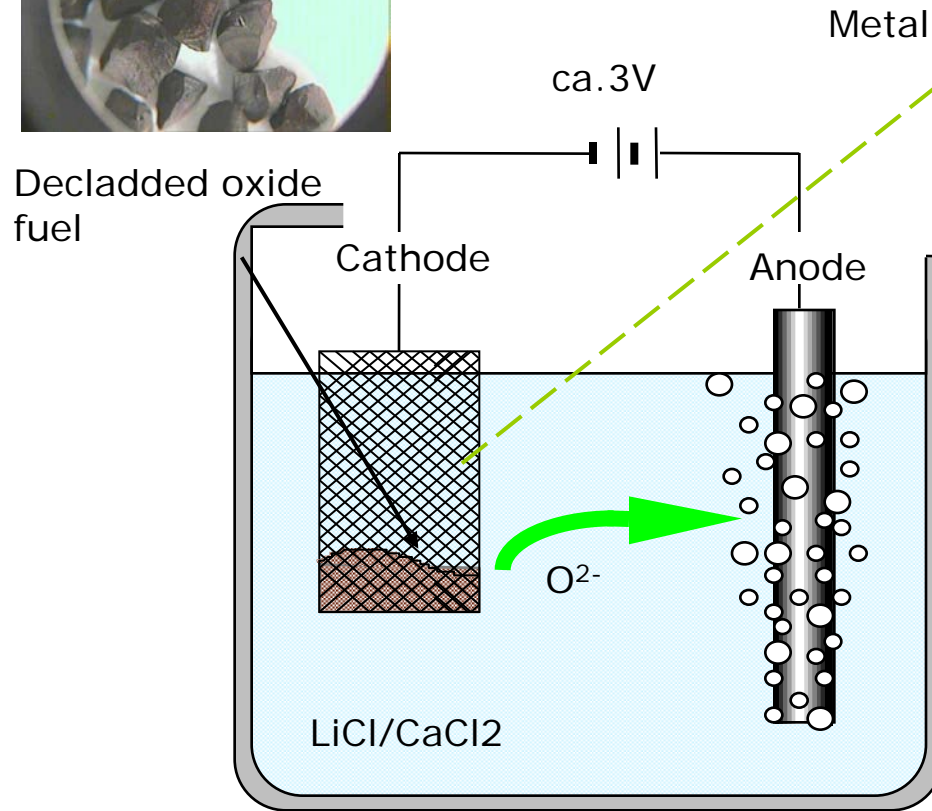
MOX 45 GWd/tHM



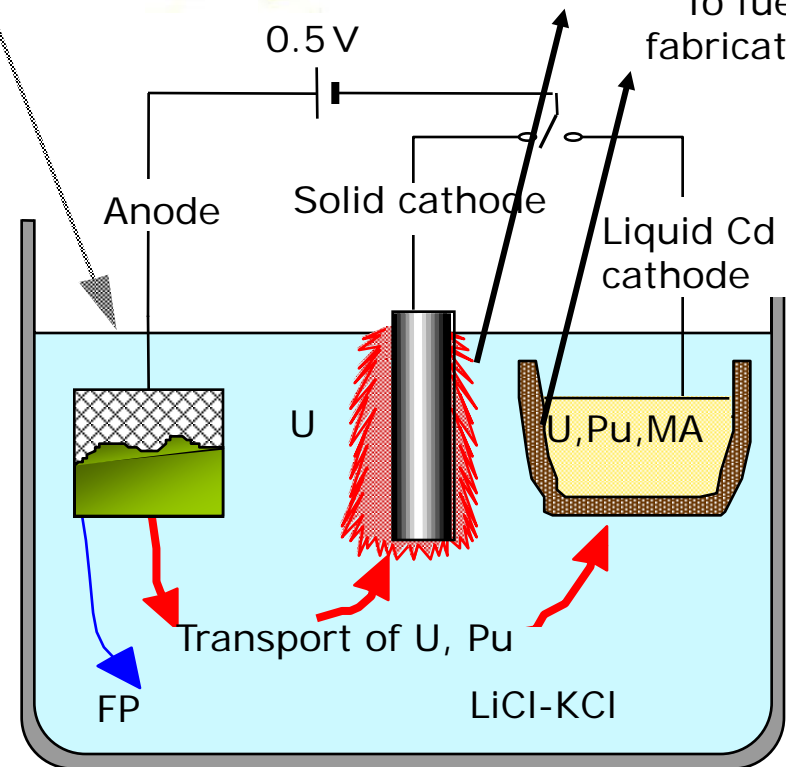
Metallic MOX

U metal deposit

To fuel fabrication



Oxide to metal conversion

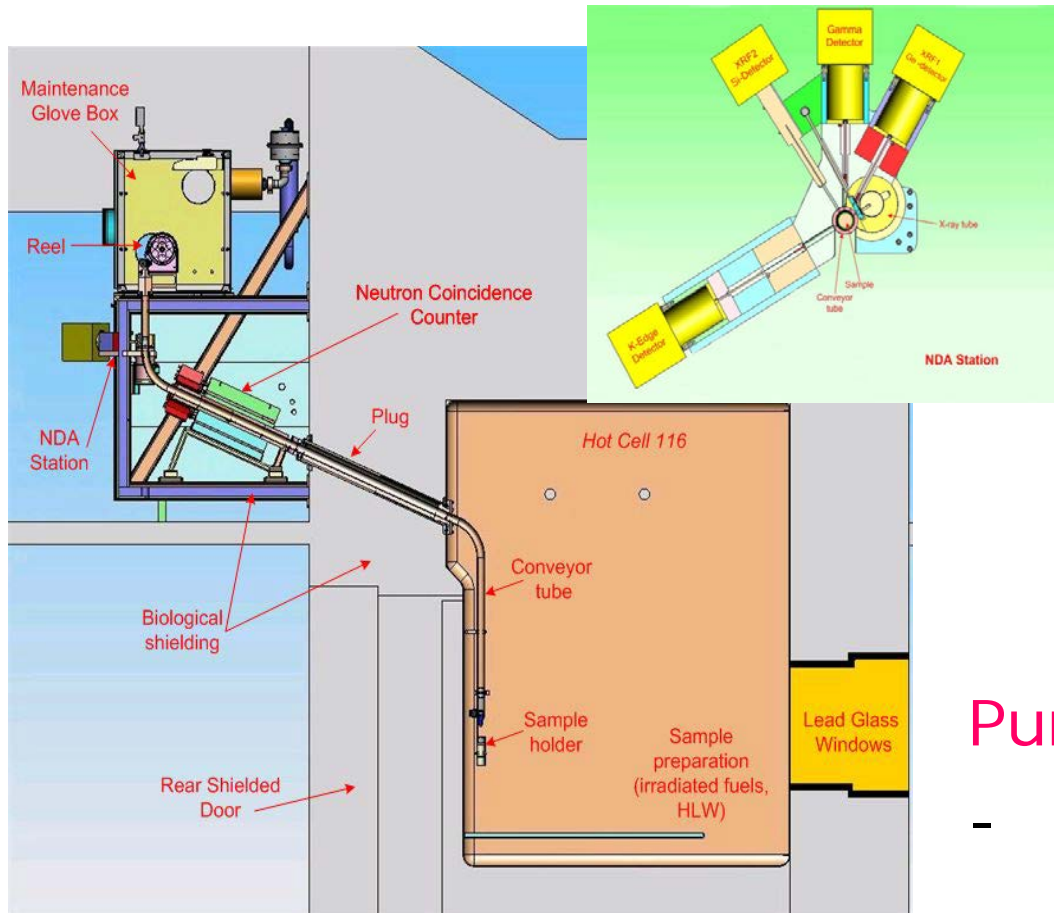


U, PU, MA refining
(FP removal)

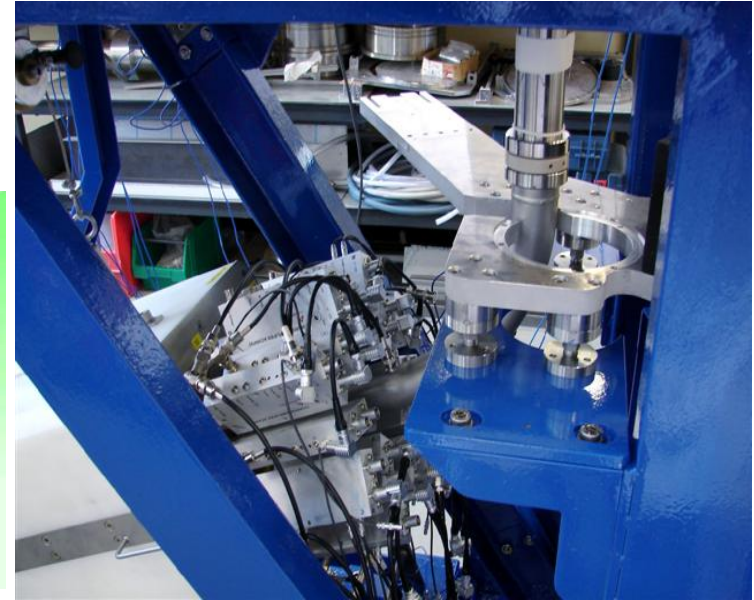
Safeguarding the pyroprocess



NDA assay system for a direct non-destructive assay on irradiated samples



Advanced NDA assay system



Testing of equipment

Purpose

- Process evaluation
- Establish a safeguard scheme

METAPHIX

Fuel Cycle Closure



fuel
characterization



U, Pu, Zr, Ln, MA
Ln, MA 0-5%



fuel fabrication

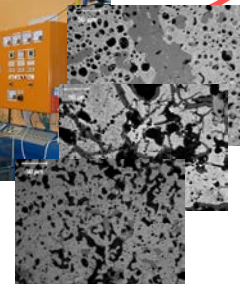


grouped actinide
separation
(U, Pu, Np, Am, Cm)



pyro-
reprocessing

post irradiation
examination



transmutation
rate ~ 10–45%
depending on
burn-up

irradiation (PHENIX)
2, 7, 11 at% burn-up





- In the SNE-TP the ESNII initiative supports a reference (SFR) and two alternative (LFR and GFR) routes as GENIV reactors systems
- Advanced closed fuel cycle demonstrated for oxide (SUPERFACT) and metallic (METAPHIX) fuel
- Transmutation in fast reactors (ASTRID) and ADS (MYRRHA) ongoing
- Homogeneous and heterogeneous minor actinide recycling options
- grouped recycling feasible for aqueous (GANEX) and dry reprocessing implies remote refabrication
- focus on a safe implementation of all of these processes